

OPTIMAL INTEGRATION OF STEAM TURBINES IN INDUSTRIAL PROCESS PLANTS

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DEFINITIONS: CHP & EFFICIENCY

- CHP = **C**ombined **H**eat and **P**ower (= energy utility system for the plant site)
- Steam Turbines are Heat Engines that operate on the Rankine cycle. They convert DP into Shaftwork; a generator then converts Shaftwork into Elec power
- Thermodynamic Efficiency is defined as

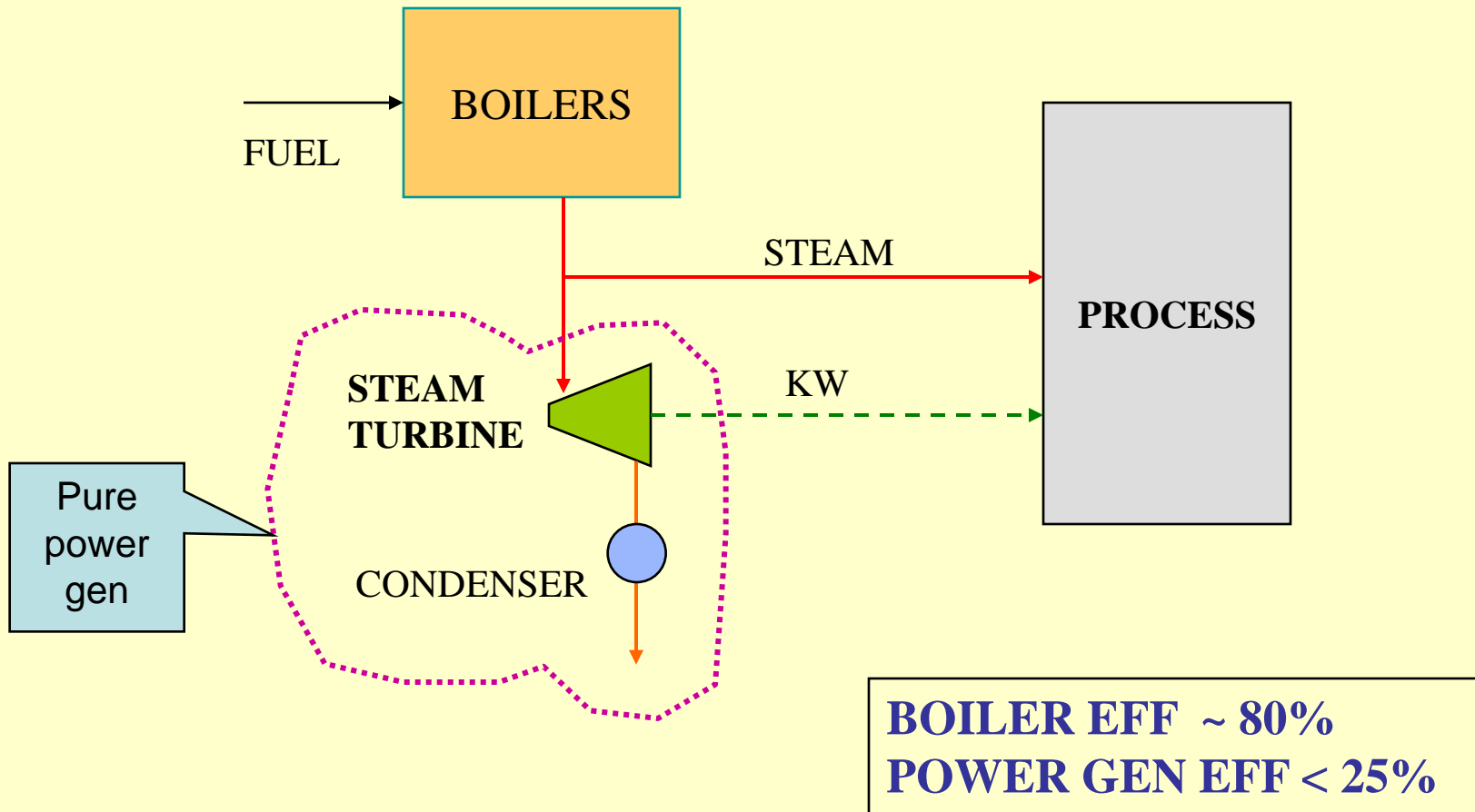
$$\frac{\text{Useful Energy Output}}{\text{Energy Input}}$$

- For Generation, 1 useful output = Power only. Machine eff = ~20%, System Eff = ~35%
- For Cogeneration, 2 useful outputs = Power + Process Heat, Machine eff = ~20%, but System Eff ~75-80%



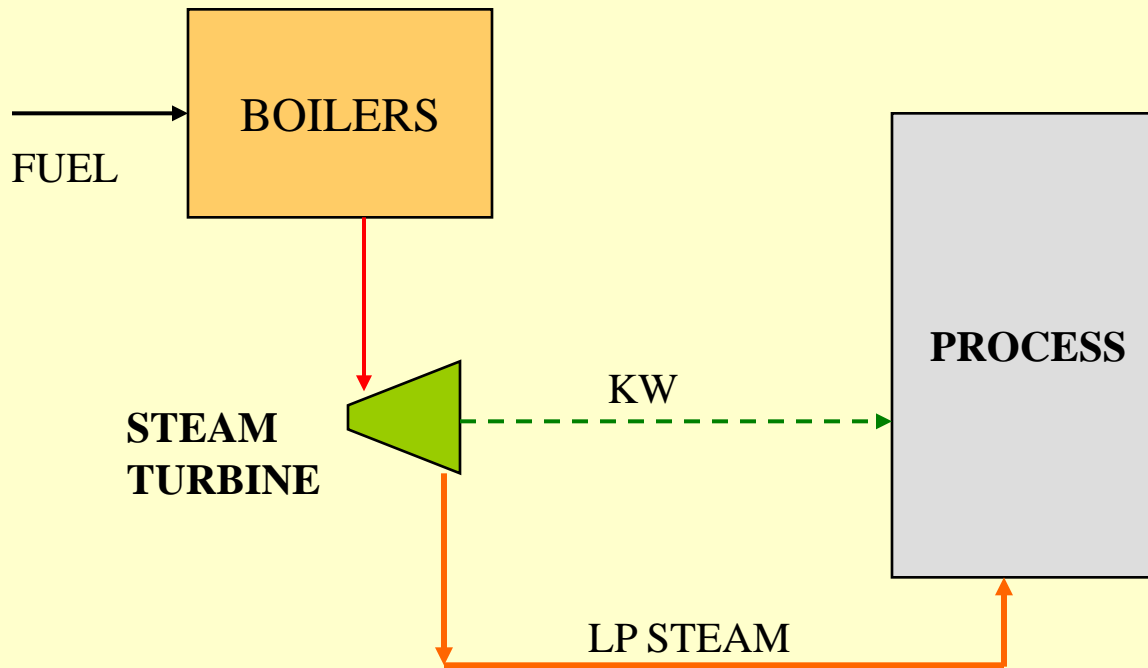
This is CHP, but not Cogeneration

LATENT HEAT OF ST EXHAUST IS WASTED



This is both CHP and “Co-Generation”

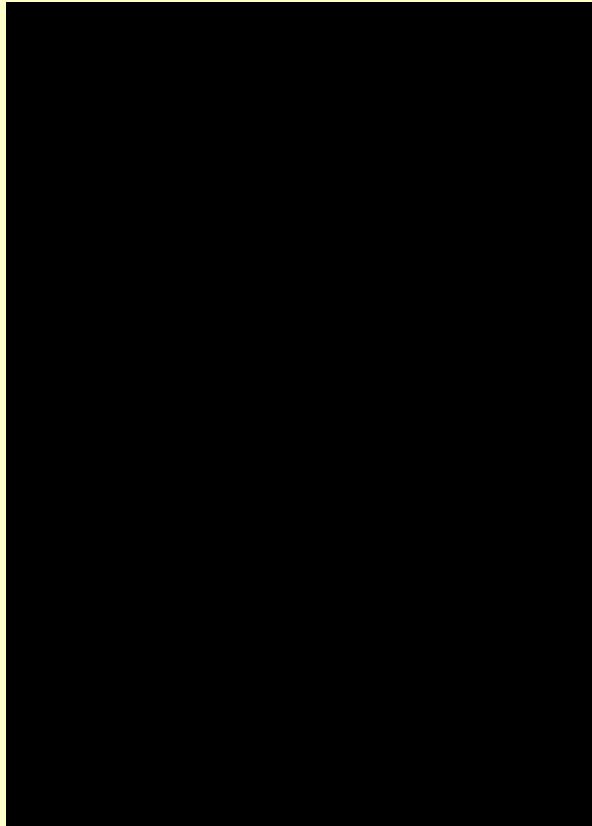
LAT HT OF EXHAUST STM IS USED IN THE PROCESS



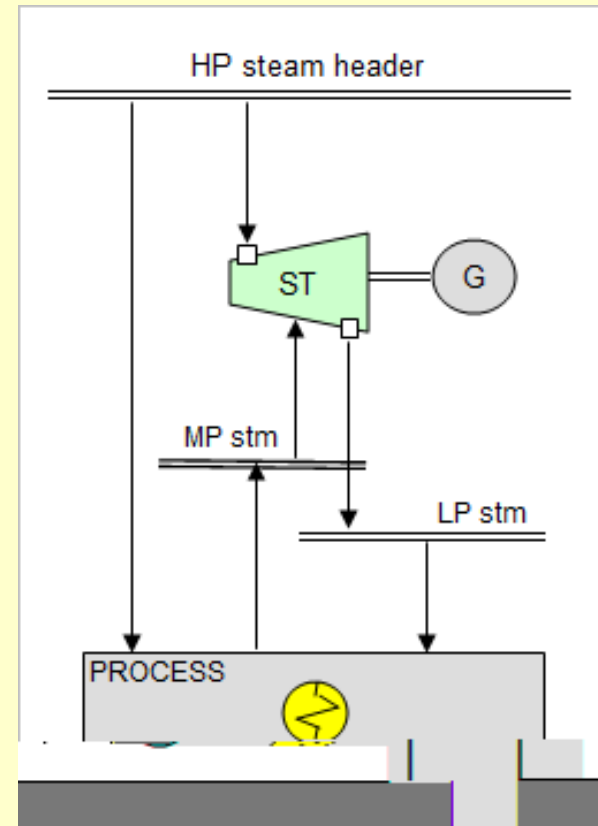
OVERALL EFF ~ 75%



Alternative Cogen configurations



Extraction Turbine



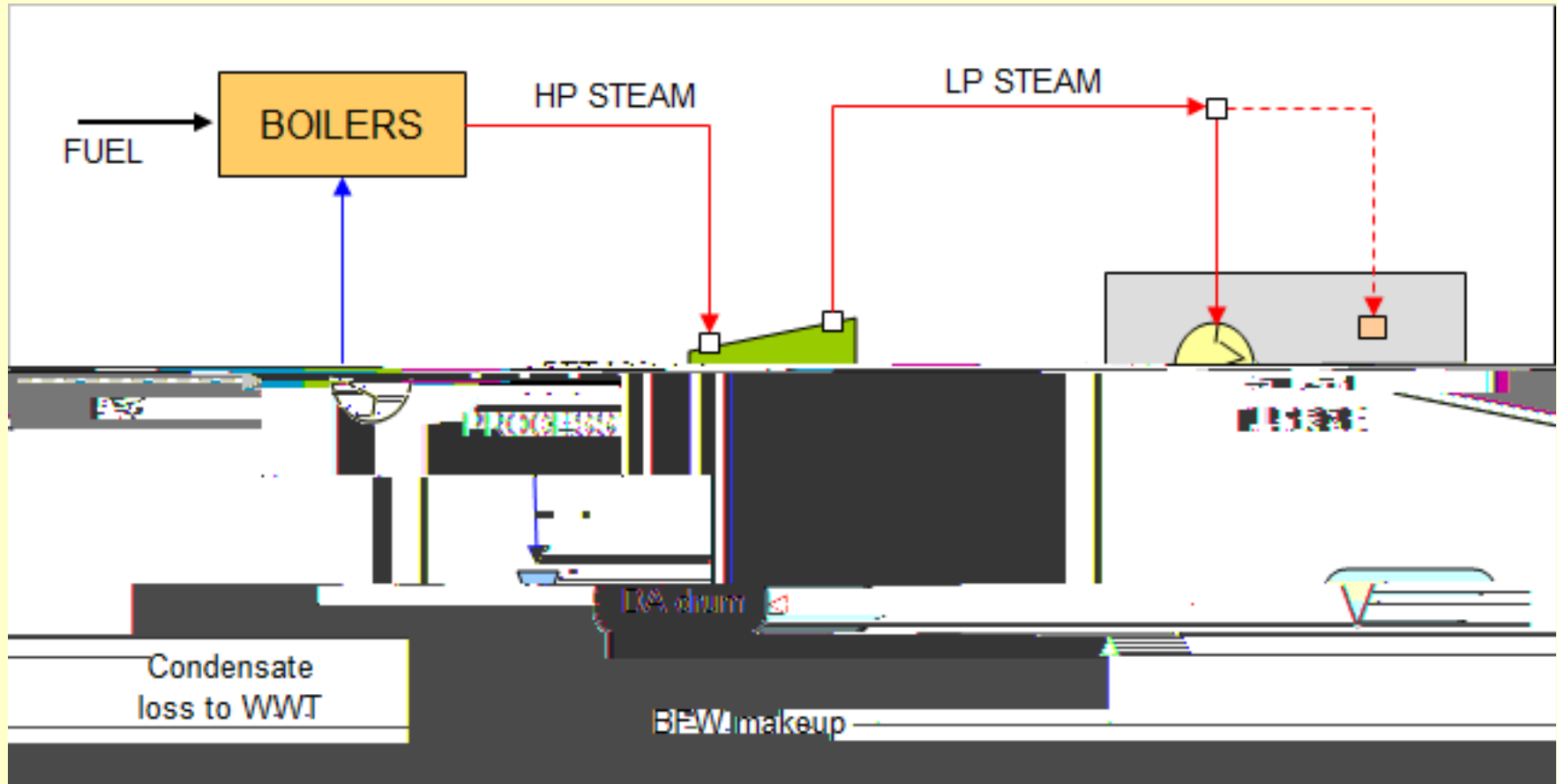
Induction Turbine



Variations – hybrid Cogen and Condensing



Simple Rankine Cycle flowsheet

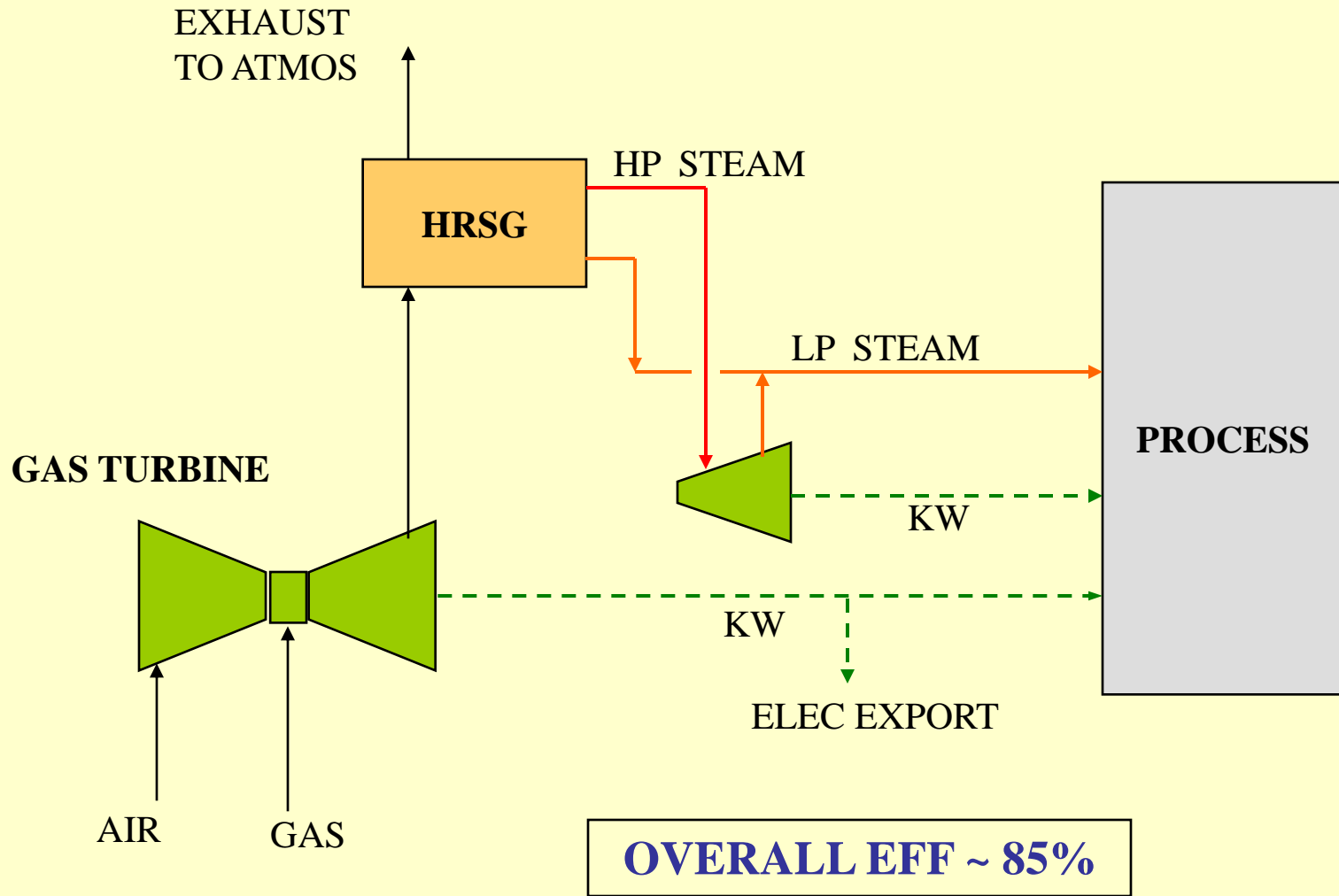


Schematic shown is for cogeneration mode

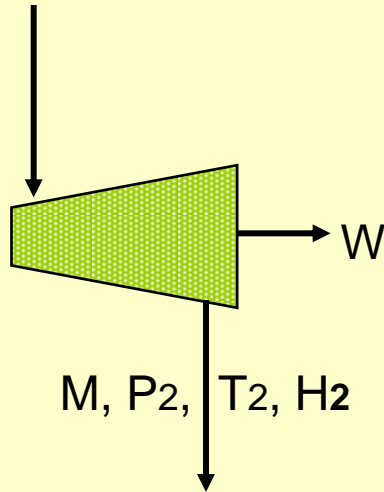




The ultimate Combined-cycle Cogen scheme



Different types of ST Efficiency



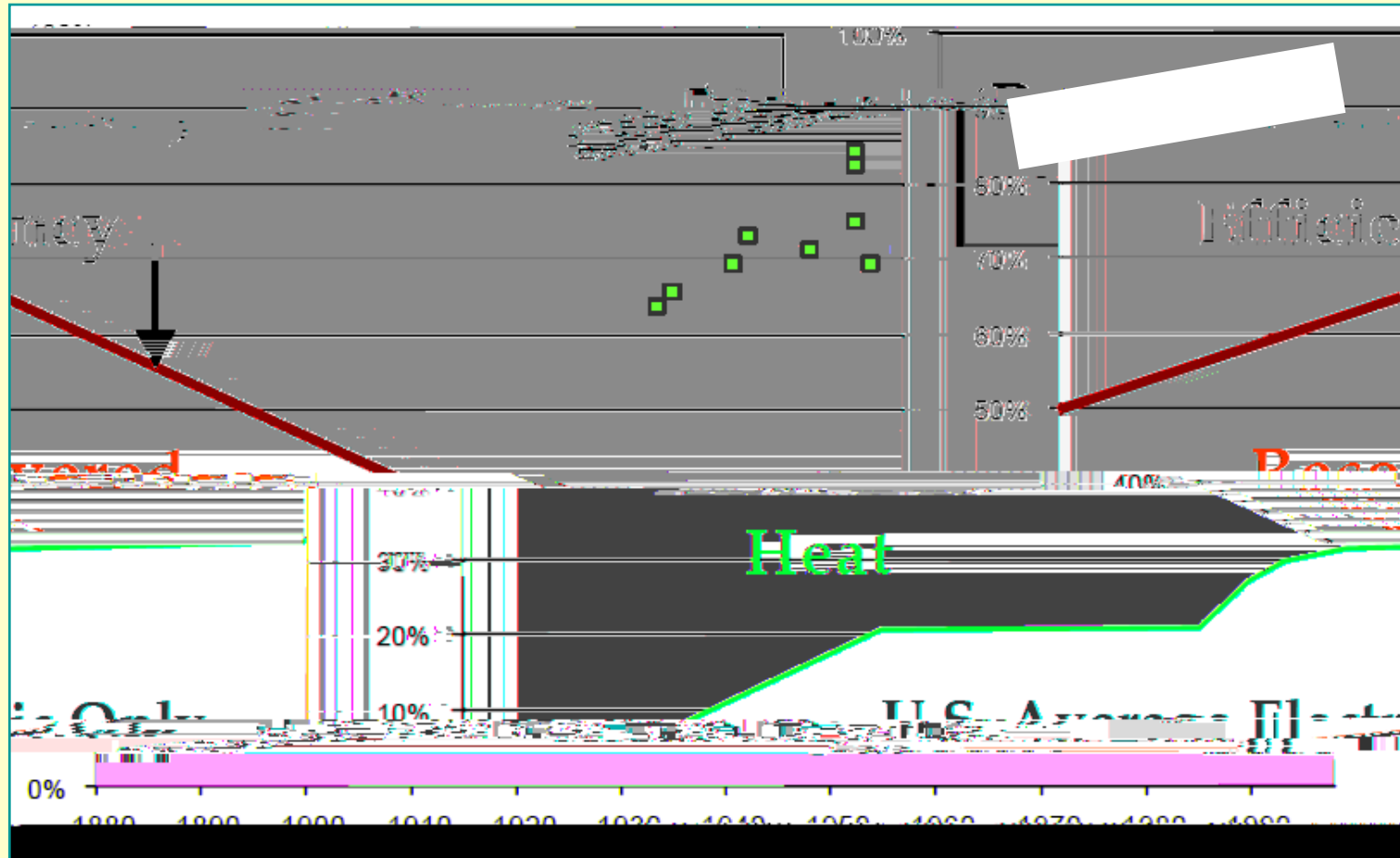
- Machine Efficiency = $W/Q_{in} = (H_1 - H_2)/H_1$
- Isentropic Efficiency = $W/[M \cdot (H_1 - H_2)_{max}] = (H_1 - H_2)/(H_1 - H'_2)$
- System efficiency

PROCESS

A rectangular box labeled 'PROCESS' with a spiral arrow inside, indicating a cyclic or continuous process. A horizontal line enters the box from the left.



A Bit of History ...

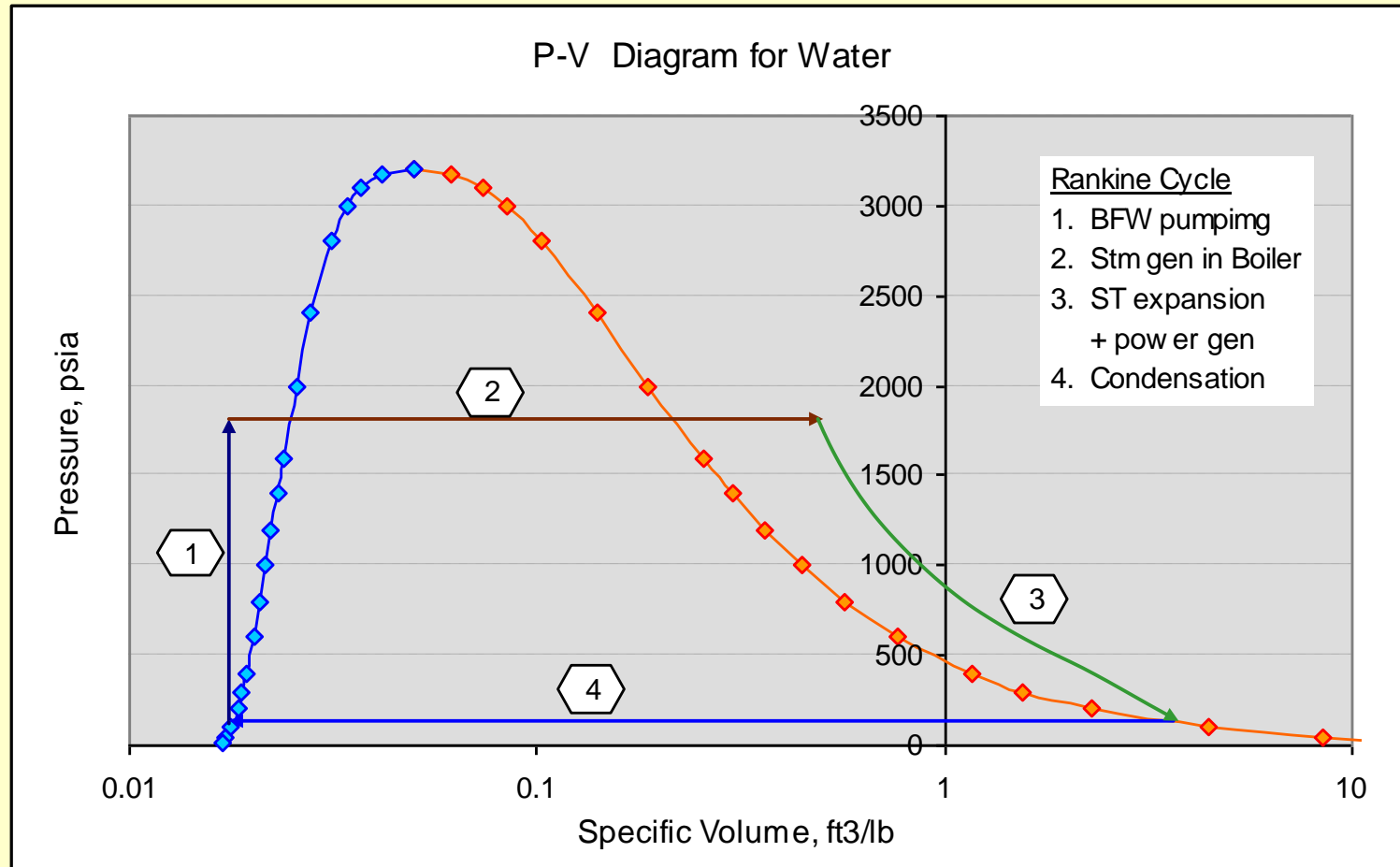


US Power plants stopped cogenerating ~1960



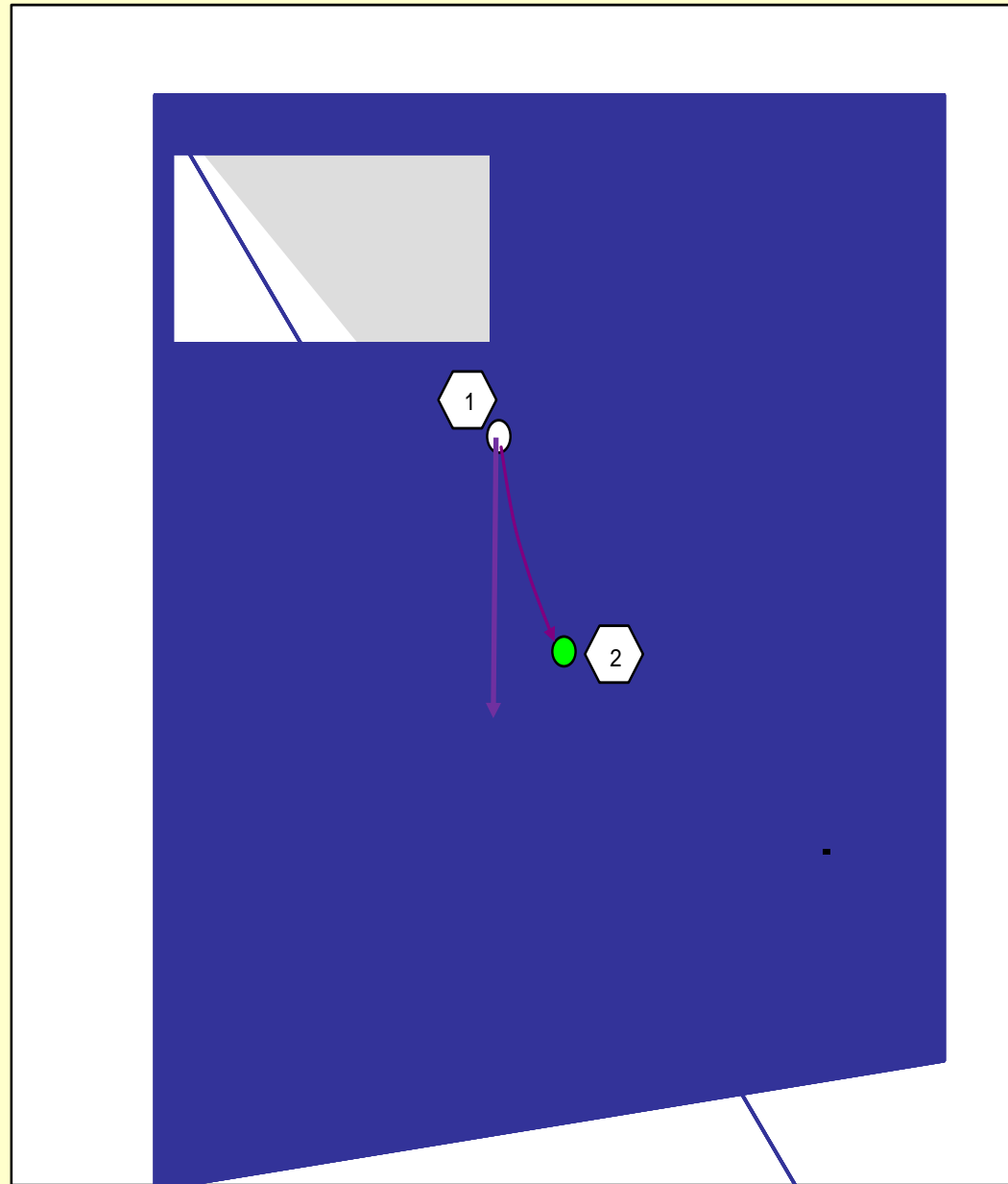
THERMODYNAMICS REVIEW

Rankine cycle on the P-V diagram



Power generation step (#3) on Mollier Chart

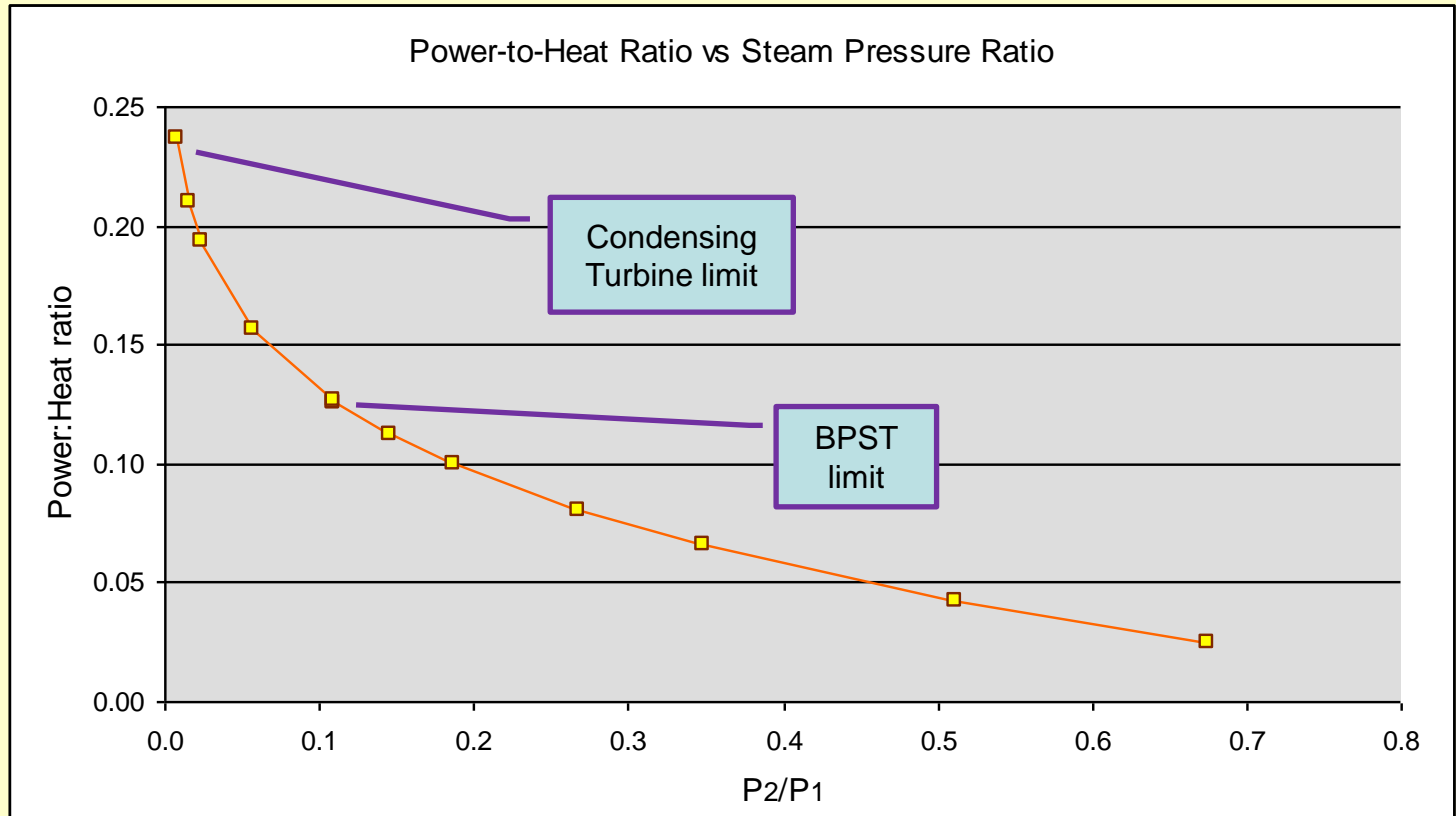
- Adiabatic expansion
(from 600 psig, 700°F to 50 psig)
- Isentropic efficiency



Effect of P_2/P_1 on Machine Efficiency (W/Q_{in})

Near-optimal
Inlet Conditions
for industrial
cogen systems

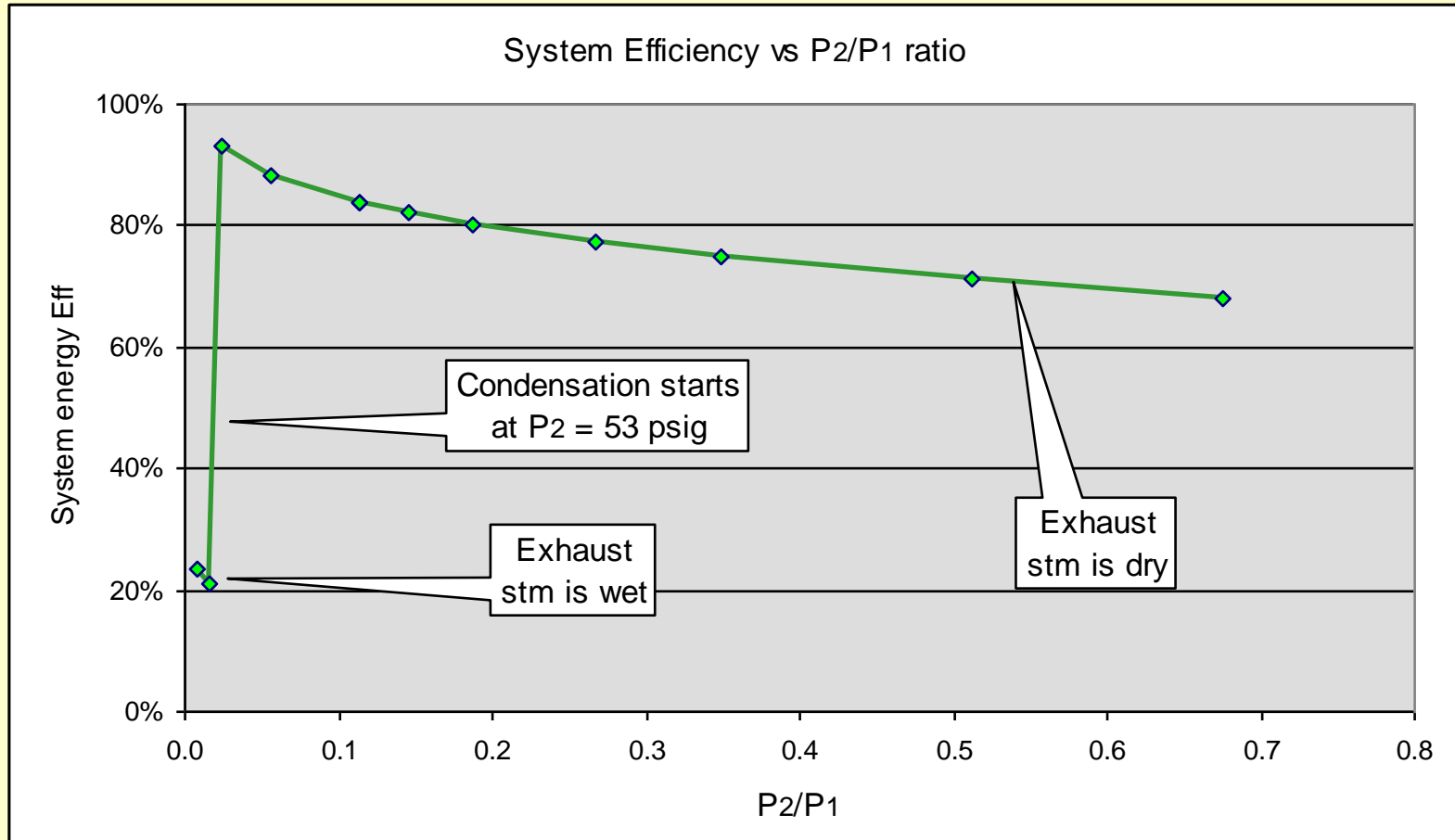
| Inlet steam | |
|-------------|---------|
| flow, lb/h | 100,000 |
| psig | 600 |
| psia | 614.7 |
| sat T | 489 |



Theoretical Machine Efficiency tops out at ~13% for BPST and 24% for CST before moisture content in turbine reaches dangerous levels.



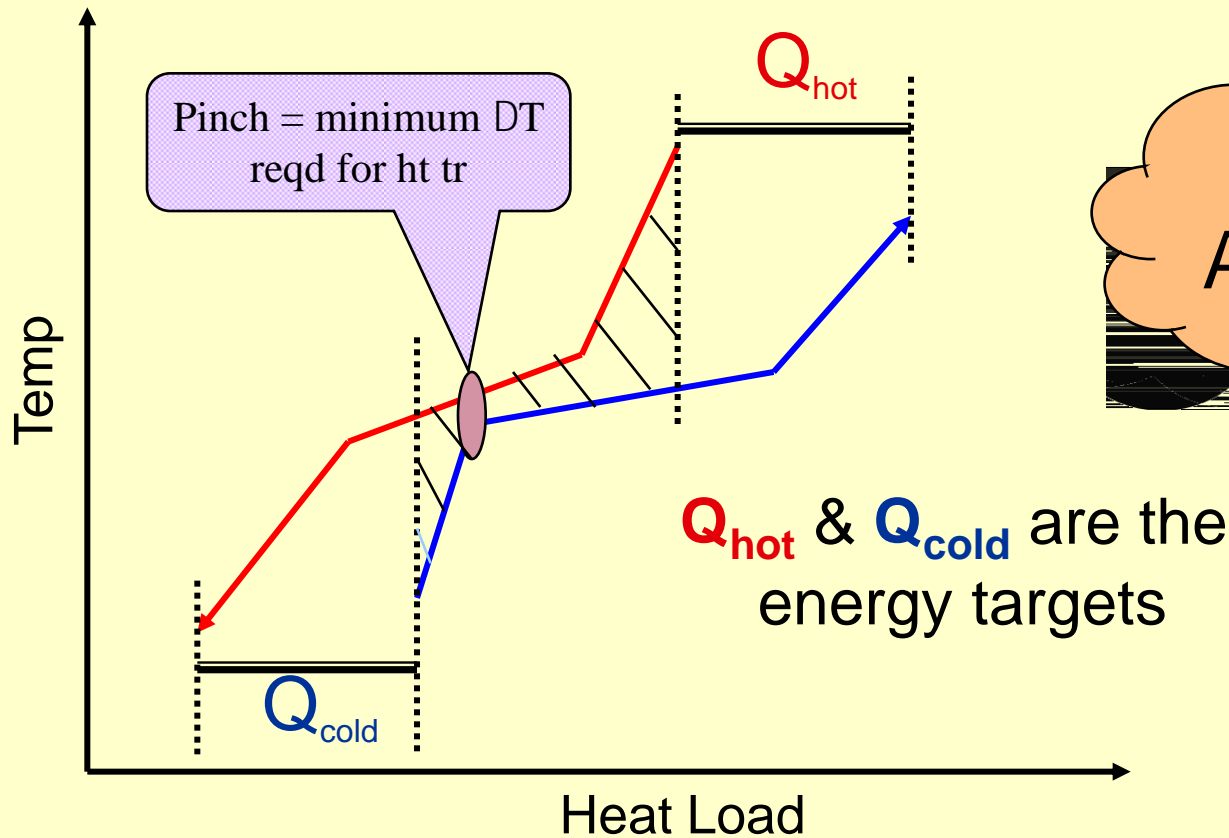
Effect of P_2/P_1 on System Efficiency



System Efficiency peaks when exhaust steam is saturated, drops rapidly as P_2/P_1 is falls, slowly as P_2/P_1 rises



OPTIMUM TURBINE INTEGRATION



It is possible to consolidate ALL the heating and cooling duties in the process into two **Composite Curves** that show the enthalpy change requirements between the entire temperature range over which the process operates



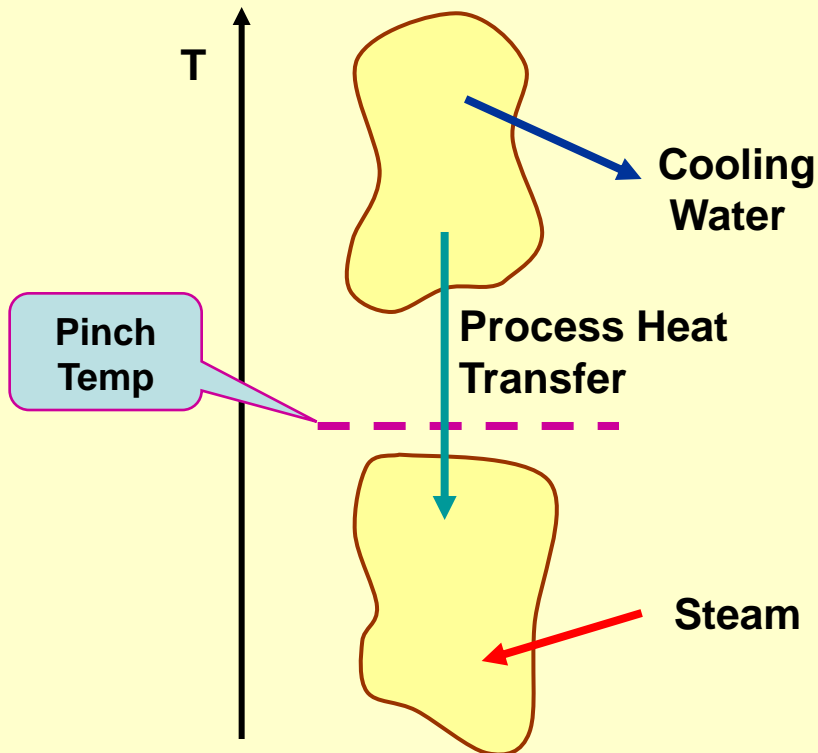
The Pinch Principle - 1

Q

If we allow **XP** heat transfer, Q_h and Q_c both increase by **XP**



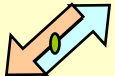
The Pinch Principle - 2



To achieve the Energy Targets, **DO NOT**

- use Steam below Pinch
- use CW above Pinch
- transfer heat from process streams above Pinch to process streams below Pinch





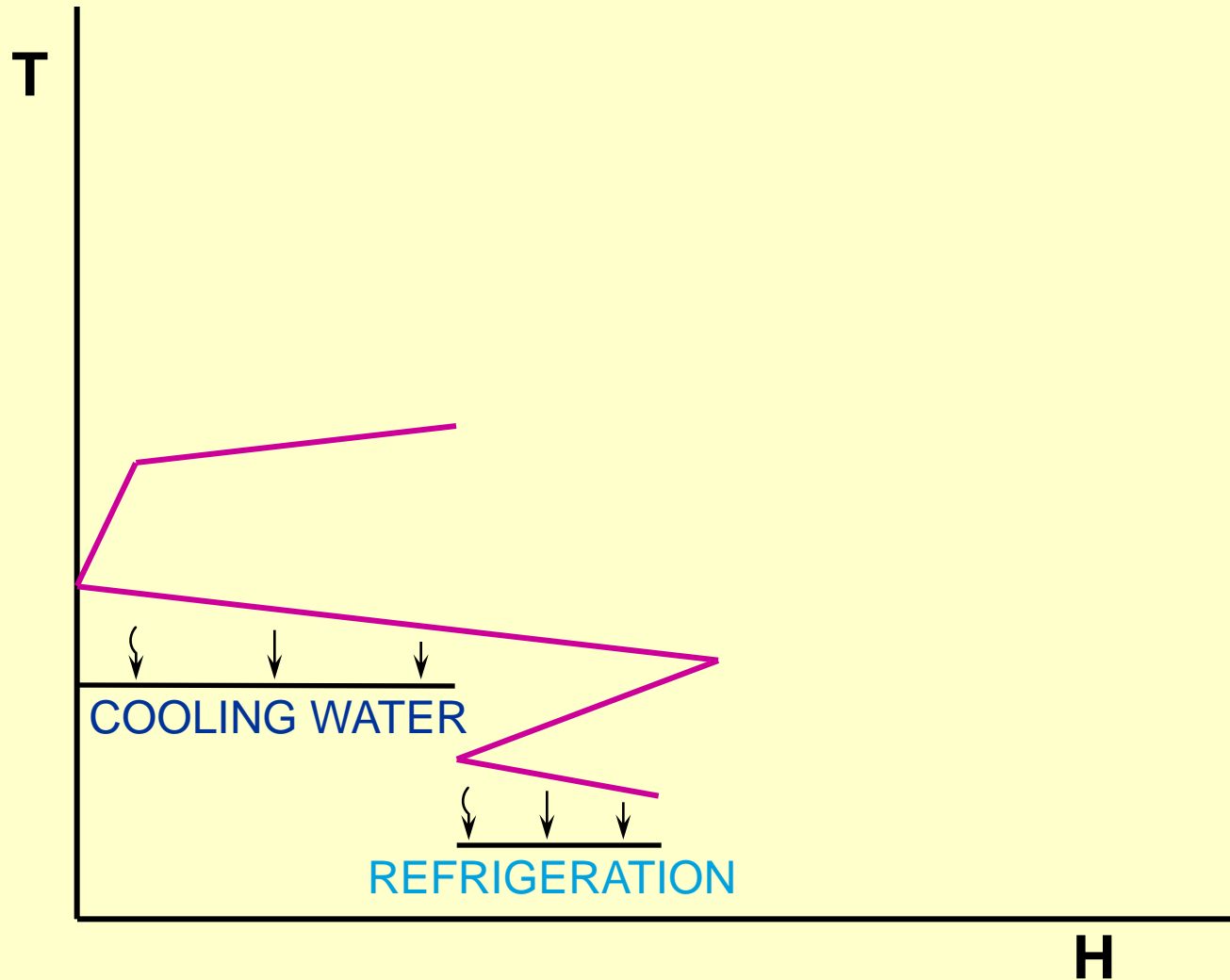
Summary of Energy Balances

| Parameter | Integrate Across PP | Integrate Above PP | Integrate Below PP |
|------------------------------------|---------------------|--------------------|--------------------|
| Process steam from fired boiler | A | A | A |
| Turbine steam from fired boiler | Q | Q | 0 |
| Turbine steam from WHB below Pinch | 0 | 0 | Q |
| Turbine exhaust vapor | $Q - W$ | $Q - W$ | $Q - W$ |
| Net HP steam required | $A + Q$ | $A + W$ | A |
| Net Total Cooling Duty | $B + (Q - W)$ | B | $B - W$ |

= Machine efficiency

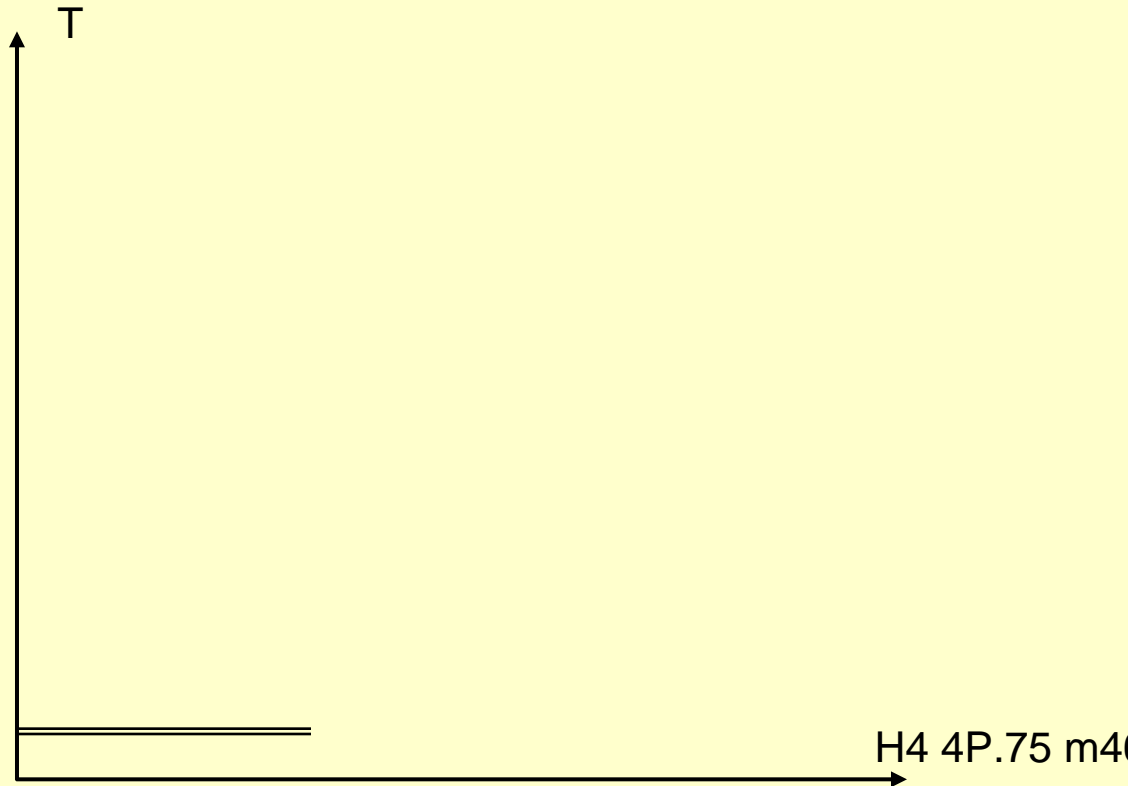


Grand Composite Curve - GCC



Correct Integration of Steam Turbine

- GCC shows us exactly how much HP and LP steam is needed, and the right P/T levels
- ST must always exhaust **ABOVE** the Process Pinch
- When designed this way, payback is very good, typically 3-4 yrs

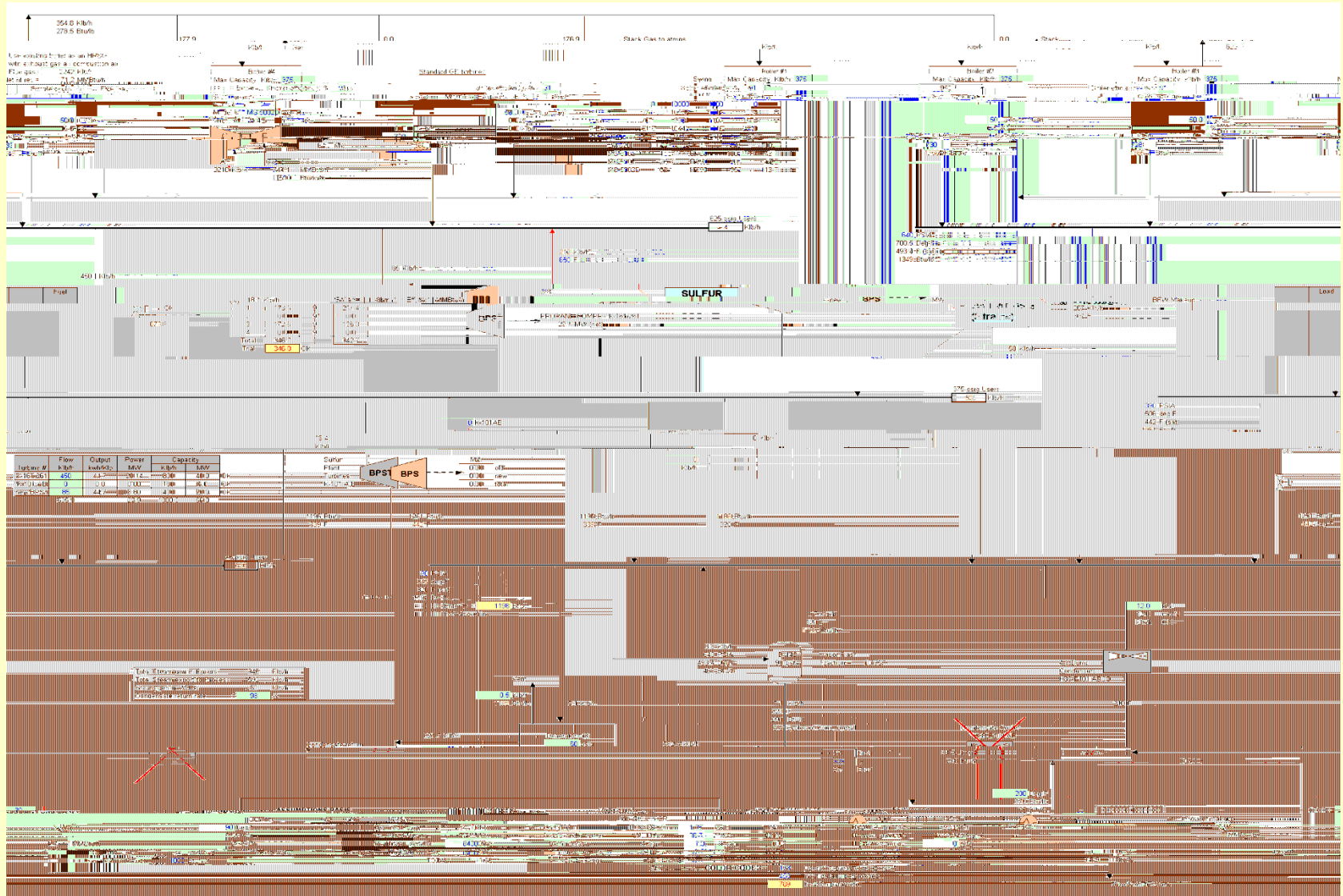


Total Site Source-Sink curves

**Net process
cooling demand
= available heat**



CHP SIMULATION MODELS



Excellent Tool for Analysis

Model should include all Key System Features:

Multiple steam levels

Multiple boilers (with eff. curves)

Process WHBs

Steam and Gas turbines (incl HRSG)

PRVs, Desuperheaters

Condensate recovery (by steam pr level)

Boiler blowdown flash & HX

Deaerators (could be > 1)

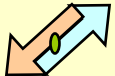
“Dump condensá á ,difM ns s »



Expected Benefits and Costs

- Typical savings = 3-5% of baseline (operator-optimized) energy costs
- Typical installed cost = \$500-900K
- Typical Payback << 1 yr
- Proven in dozens of Oil refineries, Chemical plants, Pulp/Paper mills (can be deemed a Best Practice)





Optimum Process Integration

It's like a jigsaw puzzle,
but well worth
the effort

